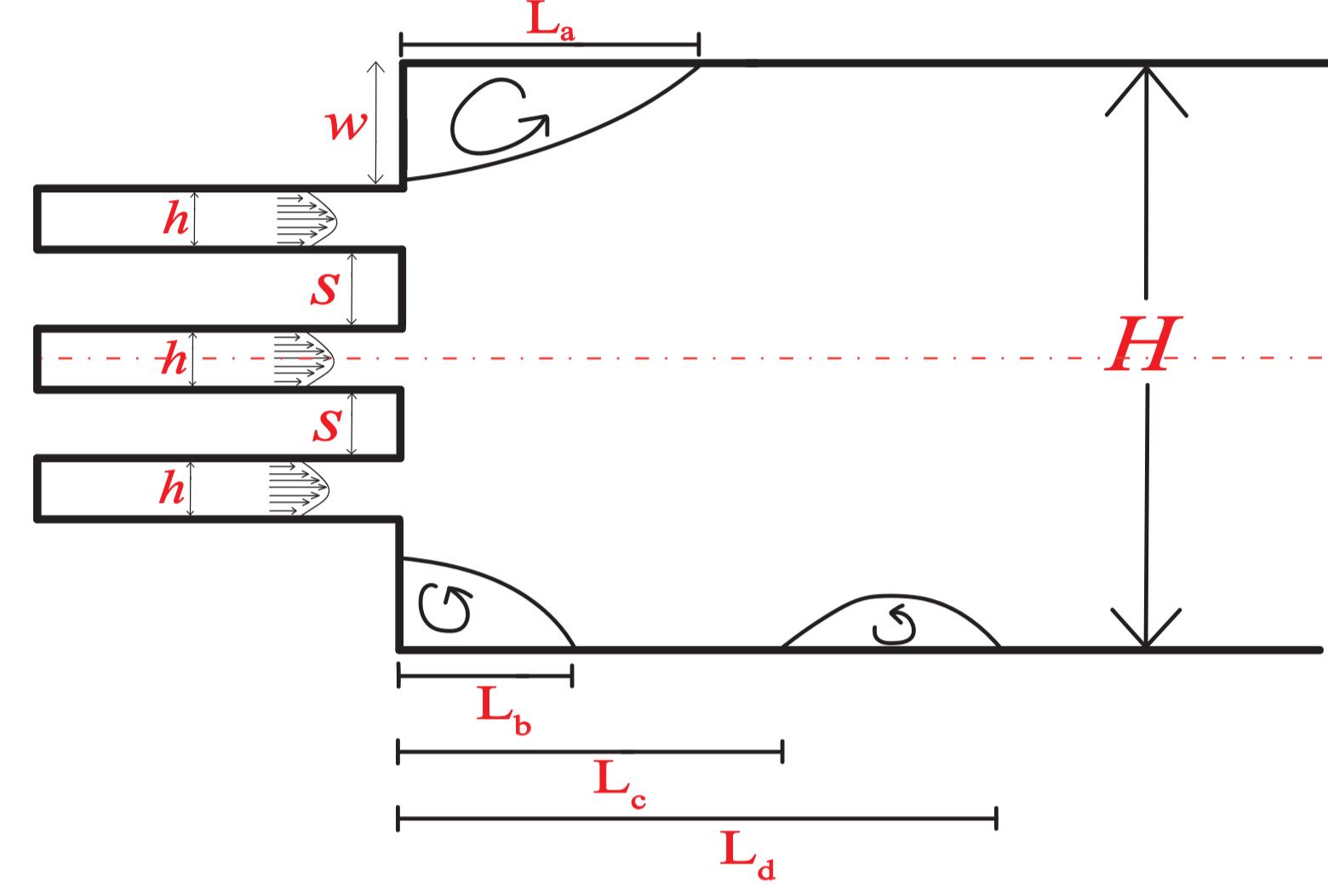


## Introduction

- **Sudden expansion** flows are ubiquitous
- **Industrial configurations** can have any number of inlets with **various spacings between inlets**
- This work aims to extend previous work on sudden expansions to a case with multiple (3) inlets
- Ostwald-De Waele (**power-law**) model and **upper-convected Maxwell** model were used to examine the influence of non-Newtonian effects
- Effect of **geometric parameters** (SR, WR), power-law index ( $n$ ) and dimensionless parameters ( $Re$ ,  $Wi$ ,  $EI$ ) on the flow were analysed

## Problem Definition & Equations



- Inlets of **equal width and equally spaced**
- Inlet spacing varied but horizontal **symmetry retained**
- Five **geometric cases** examined for 3 inlet configuration with **fixed ER = 9 (ER\* = 3)**
- All lengths **normalised by one inlet (h)**

Case	SR	WR
A	0.1	2.9
B	0.5	2.5
C (Base)	1.0	2.0
D	1.5	1.5
E	2.0	1.0

Expansion Ratio  
 $ER = H/h$   
 $ER^* = H/3h$

Spacing Ratio  
 $SR = s/h$

Wall Ratio  
 $WR = W/h$

Increased inlet spacing

## Governing Equations

$$\nabla \cdot \mathbf{u} = 0$$

$$\rho \left( \frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} \right) = -\nabla p - \nabla \cdot \boldsymbol{\tau}$$

**Mass and momentum conservation**

$$\boldsymbol{\tau} = \eta \dot{\boldsymbol{\gamma}} = (K |\dot{\boldsymbol{\gamma}}|^{n-1}) \dot{\boldsymbol{\gamma}}$$

$$Re_{gen} = \frac{6\rho \bar{u}^{(2-n)} h^n}{K \left[ \frac{4n+2}{n} \right]^n}$$

**Power-Law Model**

$$\boldsymbol{\tau} + \lambda \overset{\nabla}{\boldsymbol{\tau}} = \eta \dot{\boldsymbol{\gamma}}$$

$$Re = \frac{\rho \bar{u} h}{\eta} \quad Wi = \frac{\lambda \bar{u}}{h} \quad EI = \frac{Wi}{Re}$$

**UCM Model**

- Solved using an in-house code [1] and OpenFoam RheoTool [2]

## References and Acknowledgements

- [1] P.J Oliveira et al., J. Non-Newtonian Fluid Mechanics, **79**, 1 (1998).
- [2] F Pimenta et al., J. Non-Newtonian Fluids Mechanics, **239**, 85 (2017).
- [3] C.G Carson et al., J. Non-Newtonian Fluid Mechanics, *in press*.
- [4] S. Dhinakaran et al., J. Non-Newtonian Fluid Mechanics, **198**, 48 (2013).
- [5] R.J. Poole et al., J. Non-Newtonian Fluid Mechanics, **146**, 79 (2008).

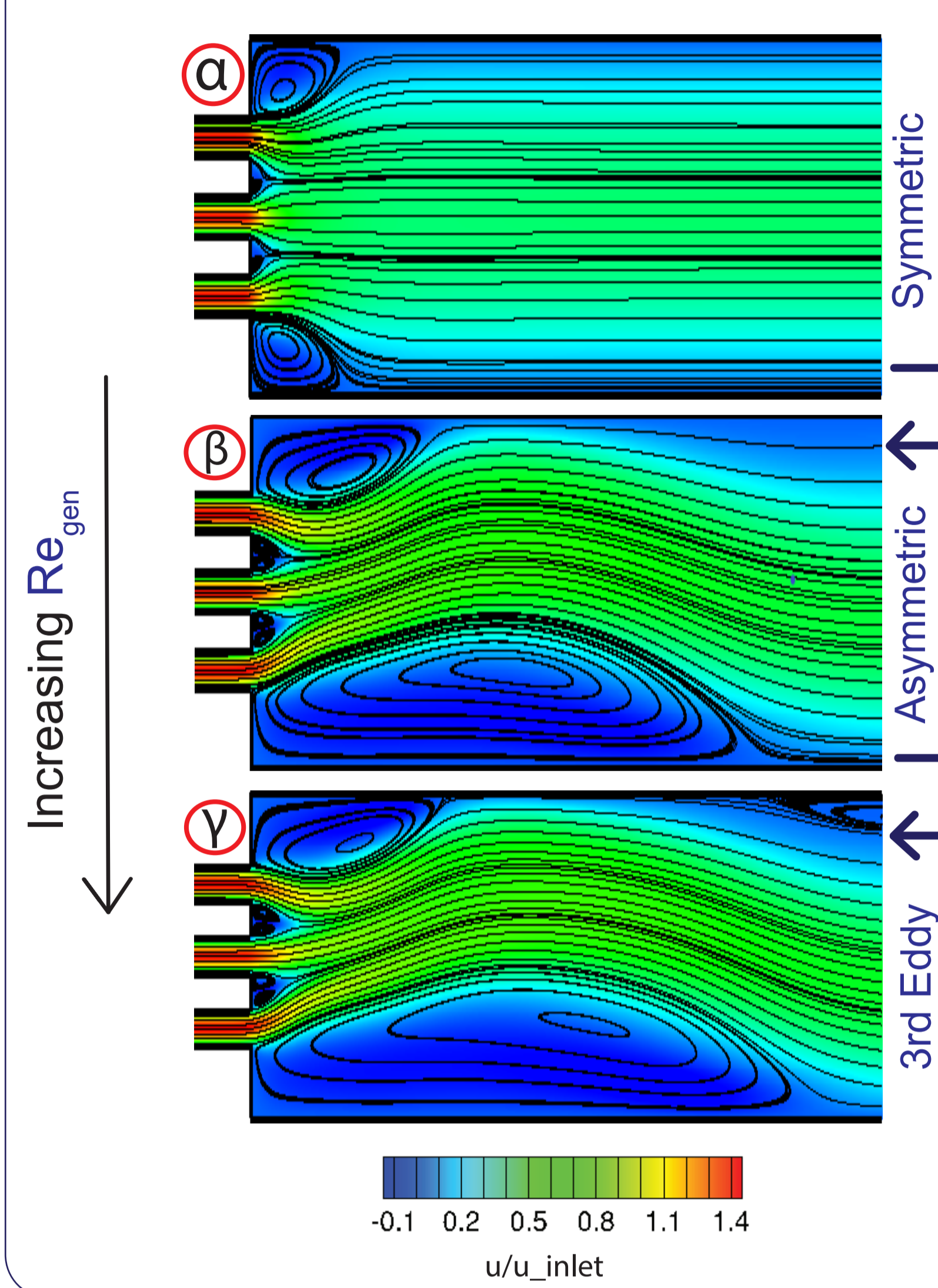
We wish to gratefully acknowledge The Society of Rheology for their generous support through The SOR Student-Member Travel Grant for ICR 2023.

We wish to acknowledge EPSRC PhD Studentship EP/W524670/1.

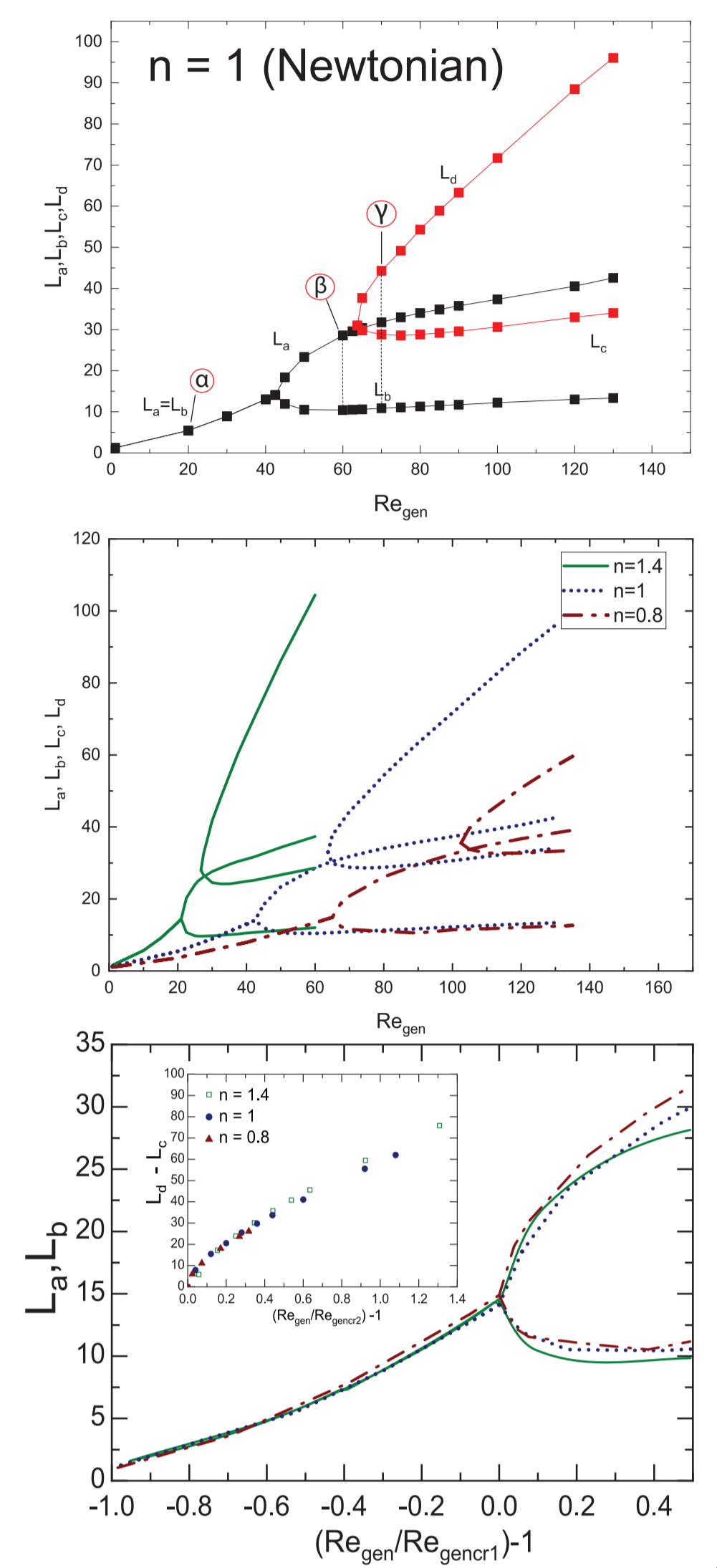
Results were obtained using the ARCHIE-WeSt High Performance Computer (www.archie-west.ac.uk) based at the University of Strathclyde.

## Results & Discussion

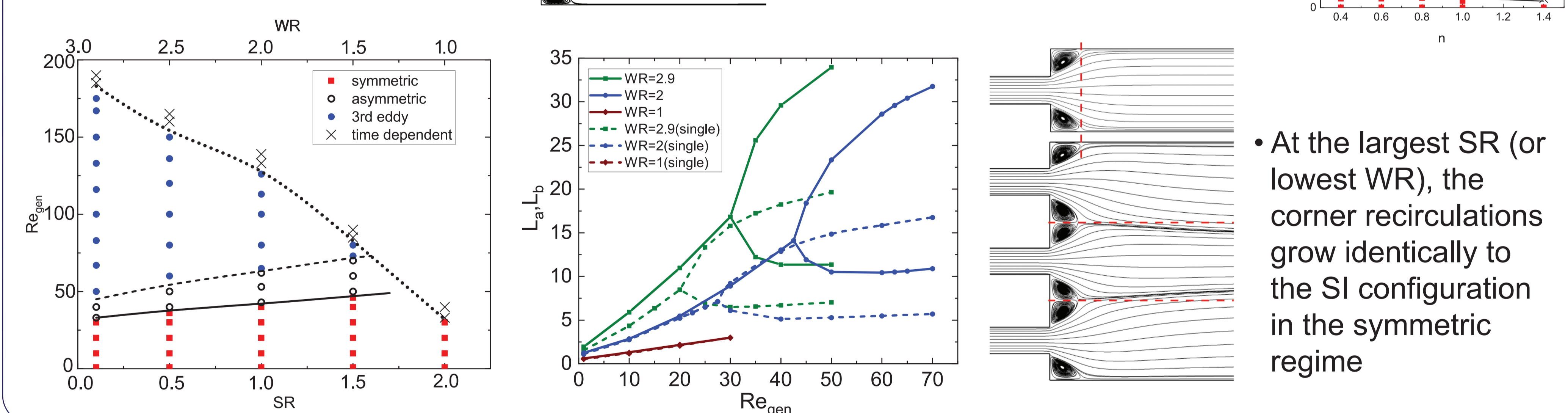
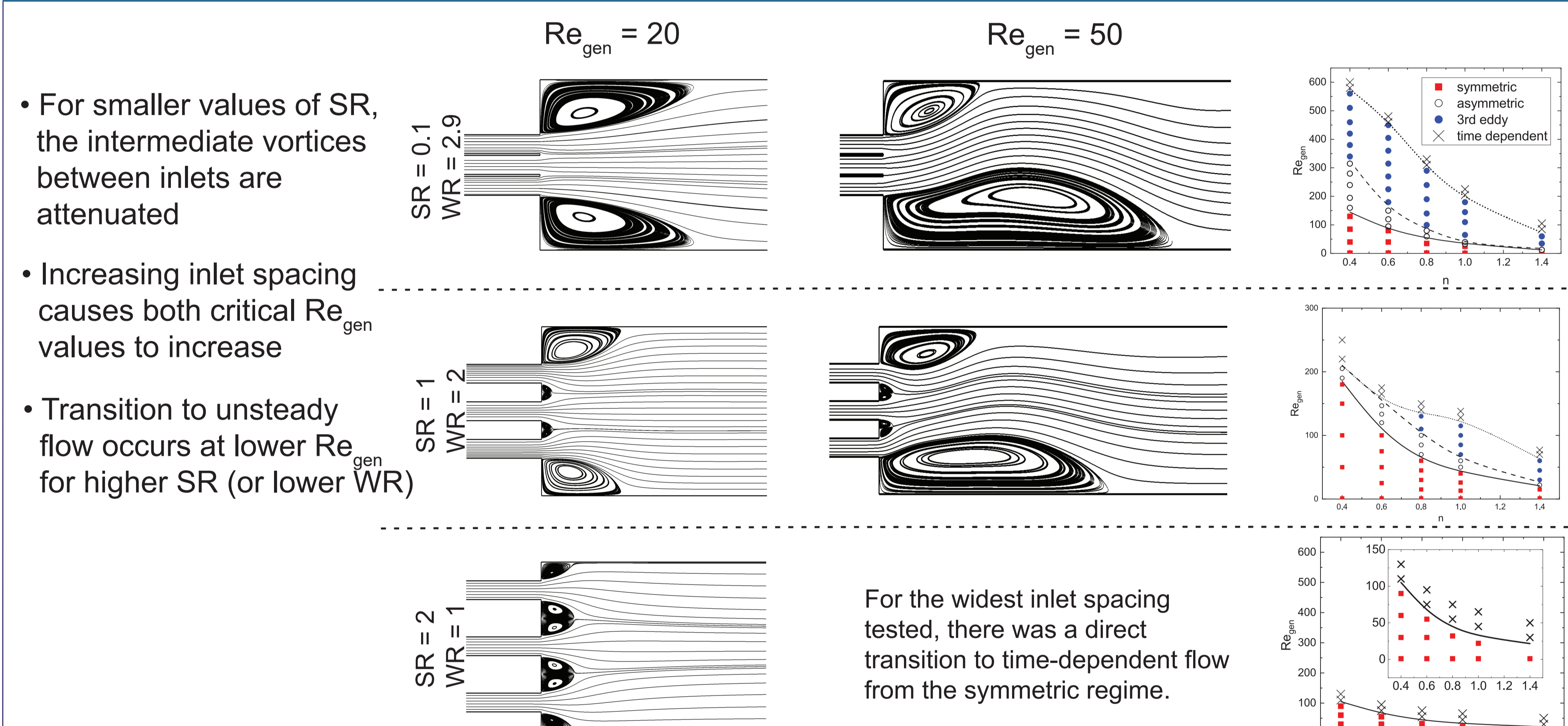
### Base Case: Power-Law Fluids [3]



- Corner recirculations and flow regimes **similar to the SI case** [4]
- In the multi-inlet case, we observe inner **recirculations between the inlets** that grow in size within the symmetric regime
- **Shear-thickening/Shear-thinning fluids** become asymmetric at **lower/higher**  $Re_{gen}$
- At asymmetric transition ( $Re_{gen,cr1}$ ), vortices are approximately equal in length and intensity for all  $n$
- New scalings help collapse the data for various values of  $n$



### Effect of Inlet Spacing



- At the largest SR (or lowest WR), the corner recirculations grow identically to the SI configuration in the symmetric regime

### Effect of Viscoelasticity

