

SUBSTITUTE GREEN SOLVENTS FOR THE PRODUCTION OF POLYMERIC MEMBRANES

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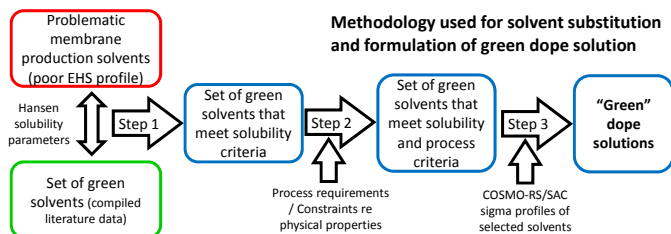
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The need for change

Environmental, Health and Safety (EHS) concerns associated with typical membrane production solvents and their placement under restrictive regulations are the driving forces behind the search for adequate alternatives also known as “green solvents”

Problematic solvents widely used in membrane manufacturing

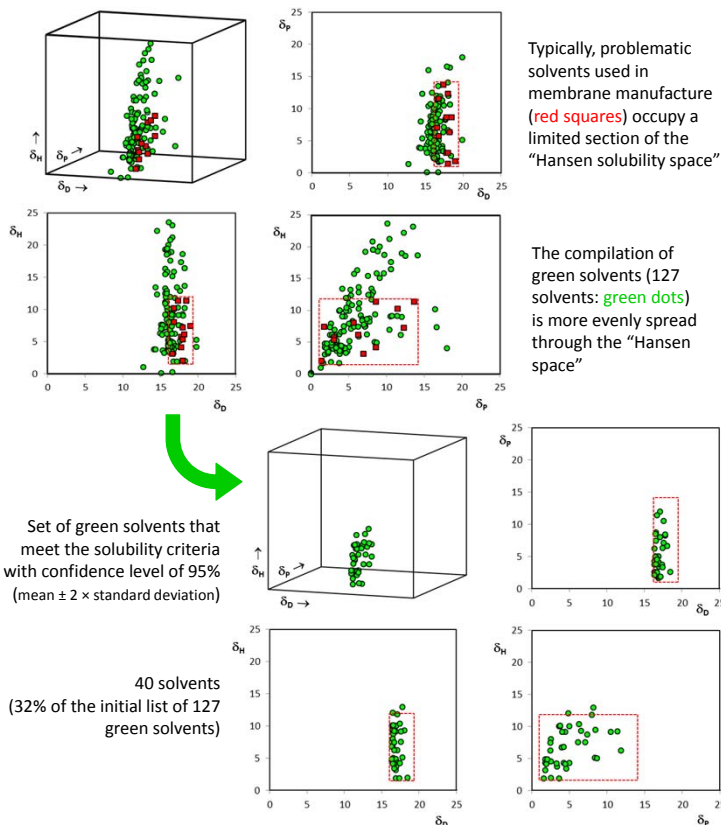
Solvent	Hansen solubility parameters, (MPa ^{1/2})			Boiling point bp (°C)
	δ_D	δ_P	δ_H	
Chloroform	17.8	3.1	5.7	61
Dichloromethane	18.2	6.3	6.1	40
Dioxane	19	1.8	7.4	101
Hexamethylphosphoramide (HMPA)	18.5	8.6	11.3	255
N,N-dimethylacetamide (DMAc)	16.8	11.5	10.2	165
N,N-dimethylformamide (DMF)	17.4	13.7	11.3	153
N-Methyl-2-pyrrolidone (NMP)	18	12.3	7.2	202
Trichloroethylene (TCE)	18	3.1	5.3	87
Tetrahydrofuran (THF)	16.8	5.7	8	67
Dibutyl phthalate (DBP)	17.8	8.6	4.1	340
Diocetyl phthalate (DOP)	16.6	7	3.1	384
Toluene	18	1.4	2	111



Step 1 – Meet solubility criteria

Approach based on the minimization of the modified difference - Ra - between the HSPs of the problematic solvent (1) and the potential substitute (2):

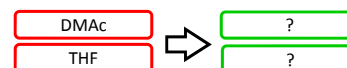
$$Ra = \sqrt{4(\delta_{D2} - \delta_{D1})^2 + (\delta_{P2} - \delta_{P1})^2 + (\delta_{H2} - \delta_{H1})^2}$$



Step 2 – Minimize process / physical properties changes

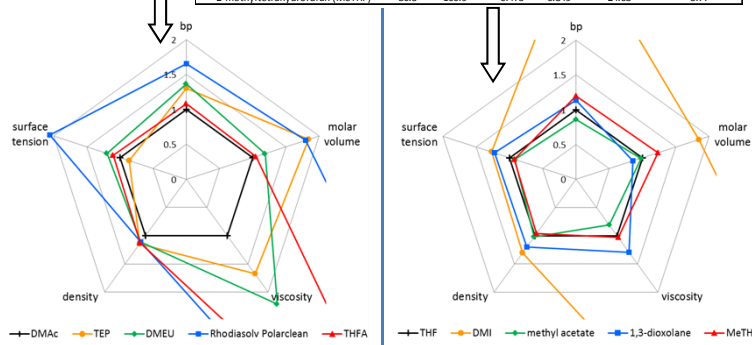
Physical properties of the solvents such as boiling point, molar volume, water miscibility, viscosity, density and surface tension can affect the membrane production process and must also be considered in the evaluation process

Case study: polymeric dope solutions containing DMAc and THF used for dry-wet spinning of polysulfone hollow fibre membranes



	bp (°C)	molar volume [cm ³ /mol]	viscosity [mPa.s]	density [g/cm ³]	surface tension [mN/m]	“Hansen” distance Ra [(MPa) ^{1/2}]
N,N-Dimethylacetamide (DMAc)	165	92.5	0.93	0.933	33.53	-
Triethylphosphate (TEP)	215	170.6	1.56	1.068	28.98	1.02
N,N'-Dimethylethylenurea (DMEU)	225	109.8	2.06	1.040	40.1	2.18
methyl 5-(dimethylamino)-5-oxopentanoate (Rhodiasolv Polarclean)	273	166.7	9.78	1.039	69.00	3.16
tetrahydrofurfuryl alcohol (THFA)	178	97.3	5.35	1.050	37	4.71

	bp (°C)	molar volume [cm ³ /mol]	viscosity [mPa.s]	density [g/cm ³]	surface tension [mN/m]	“Hansen” distance Ra [(MPa) ^{1/2}]
tetrahydrofuran (THF)	67	81.7	0.46	0.882	26.5	-
dimethyl isosorbide (DMI)	236	151.2	5	1.150	33.7	2.18
methyl acetate	57.5	79.7	0.37	0.898	24.41	3.03
1,3-dioxolane	76	69.9	0.596	1.059	32.55	3.04
2-methyltetrahydrofuran (MeTHF)	80.3	100.9	0.475	0.849	24.68	3.77



Step 3 - “Green” dope formulation

Case study

Typical dope solution composition

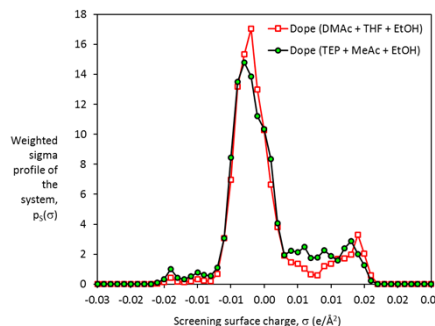
Component	% wt
Polysulfone	22
DMAc	32
THF	32
Ethanol	14

Potential substitution



Approach based on:

- Conductor-like Screening Model for Real solvents (COSMO-RS) and the variant COSMO – SAC
- Database of sigma profiles compiled by Liu and co-workers at Virginia Tech (Mullins et al., 2006)



Composite sigma profile for the system / dope is given by the weighted sum of the sigma profiles of the individual solvents (Klamt and Eckert, 2000)

Novel dope composition is obtained by minimizing the differences between the original and the “new” weighted sigma profiles

Component	wt %
Polysulfone	22
TEP	39.7
Methyl Acetate	8.1
Ethanol	30.1

Main references:

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