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Flow of deformable droplets: discontinuous shear thinning and velocity oscillations

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We study the rheology of a suspension of soft deformable droplets subjected to a pressure-driven flow. Through computer simulations, we measure the apparent viscosity as a function of droplet concentration and pressure gradient, and provide evidence of a discontinuous shear thinning behaviour, which occurs at a concentration-dependent value of the forcing. We further show that this response is associated with a nonequilibrium transition between a ‘hard’ (or less deformable) phase, which is nearly jammed and flows very slowly, and a ‘soft’ (or more deformable) phase, which flows much more easily. The soft phase is characterised by flow-induced time dependent shape deformations and internal currents, which are virtually absent in the hard phase. Close to the transition, we find sustained oscillations in both the droplet and fluid velocities. Polydisperse systems show similar phenomenology but with a smoother transition, and less regular oscillations.

Concentrated suspensions of colloidal particles in a liquid solvent are often found in industry and nature. Familiar examples include paint, ink, food like mayonnaise and ice cream, and biological fluids such as blood \cite{1}. The flow properties of colloidal suspensions can be distinctively non-trivial: for example, a suspension of colloidal spheres in water first exhibits shear thinning and then shear thickening, as the external forcing (pressure gradient or shear) is increased \cite{15}. In dense suspensions, the fact that shear thickening can be discontinuous has recently attracted a lot of attention: this behaviour marks a transition between a lubrication-dominated and a frictional flow regime \cite{5}.

Often, in such colloidal fluids, the dispersed particles are not hard, but soft, and deformable \cite{6}. Examples are the fat droplets found in milk, or eukaryotic cells: all these can deform under flow, or when subjected to a mechanical stress. While hard sphere fluids have been studied extensively, and provide the basis for our understanding of the glass transition \cite{7,9}, and of soft glassy rheology \cite{10}, less is known about the flow response of suspensions of deformable particles \cite{6,11,15}. Nonetheless, there is a number of examples suggesting that the physics of soft suspensions is both highly interesting and important in applications. For example, experiments and simulations have recently demonstrated that glass transitions and jamming can be observed in dense monolayers of living cells \cite{16–19}. Emulsions – which are dispersion of liquid droplets in a continuous medium – are also used in medicine and food, and their flow properties play a pivotal role in applications. Particle deformability is important to determine the rheology of a material: for example, emulsions and foams do not normally display shear thickening, unlike hard sphere colloidal fluids.

Here, we use 2D lattice Boltzmann simulations to investigate the dynamics of a suspension of soft, and non-coalescing, droplets (Figs. 1a,b) under pressure-driven flow within a channel. Two key parameters determine the flow response of our system: (i) the concentration, $\Phi$, defined as the ratio between the area of all droplets and the total area of the simulation domain, and (ii) the applied pressure difference $\Delta p$ driving the flow. We calculate the apparent viscosity, $\eta$, of the suspension as a function of $\Phi$ and $\Delta p$ – this is the focus of the current paper, in contrast to previous numerical works on droplet rheology \cite{11–13}. As expected, we find that, for a fixed $\Delta p$, $\eta$ increases sharply with $\Phi$, as droplets approach jamming. The behaviour of $\eta$ with $\Delta p$ is more surprising, and constitutes our central result: if the concentration is large enough, we find $\eta$ shows discontinuous shear thinning rheology. This non-Newtonian behaviour signals a nonequilibrium (flow-induced) transition between a ‘hard’ (or less deformable) phase, where the flow does not appreciably affect droplet shape, and a ‘soft’ (or more deformable) phase, where the droplets deform substantially, in a time-dependent fashion. Close to the transition, we find strong and sustained oscillations in the velocity of the droplets (or of the underlying fluid). These oscillations are strikingly similar to those observed for hard colloidal particles under Poiseuille flow \cite{20}. In our case, the underlying mechanism is the proximity to the discontinuous shear-thinning transition, which leads to unabating hopping between the hard and soft viscosity branches. Discontinuous shear thinning and oscillations are more easily seen in a monodisperse suspension: in a binary system with droplets of two different sizes the transition is much smoother, more akin to a crossover.

To study the hydrodynamics of our soft droplet fluid, we follow the evolution of: (i) phase-field variables describing the density of each of the droplets, $\phi_i$, $i = 1, \ldots, N$, where $N$ is the total number of droplets, and (ii) the velocity field of the underlying solvent $v$. The equilibrium behaviour is governed by the following free energy density,

$$f = \frac{\alpha}{4} \sum_{i=1}^{N} \phi_i^2 (\phi_i - \phi_0)^2 + \frac{K}{2} \sum_{i=1}^{N} (\nabla \phi_i)^2 + \epsilon \sum_{i,j,i<j} \phi_i \phi_j.$$  \hspace{1cm} (1)
In Eq. 1, the first two terms ensure that each droplet is stable, as, for every $i$, $\phi_i = \phi_0$ inside the $i$-th droplet, and 0 otherwise; these two terms also determine the surface tension of each of the droplets as $\gamma = \sqrt{(8K\alpha)/9}$ and their interfacial thickness as $\xi = 5\sqrt{K/(2\alpha)}$ [21]. The third, final term describes soft repulsion pushing droplets apart when they overlap: $\epsilon > 0$ controls the strength of this repulsion.

The dynamics of the compositional order parameters $\{\phi_i\}_{i=1,\ldots,N}$ evolve according to a set of Cahn-Hilliard-like equations,

$$\frac{\partial \phi_i}{\partial t} - \nabla \cdot (\mathbf{v} \phi_i) = M\nabla^2 \phi_i + \frac{\partial f}{\partial \phi_i}$$

(2)

where $M$ is the mobility and $\mu_i = \partial f/\partial \phi_i - \partial_f \phi_i/\partial (\partial \phi_i)$ is the chemical potential of the $i$-th droplet. Eq. 2 conserves the area of each of the droplets (i.e., the integral of each $\phi_i$ over the whole simulation domain).

The solvent flow obeys the Navier-Stokes equation,

$$\rho \left( \frac{\partial \mathbf{v}}{\partial t} + \mathbf{v} \cdot \nabla \mathbf{v} \right) = -\nabla p + \sum_{i} \phi_i \nabla \mu_i + \eta_0 \nabla^2 \mathbf{v},$$

(3)

where $\rho$ indicates the fluid density, $p$ denotes its pressure and $\eta_0$ the solvent viscosity. The term $\sum_{i} \phi_i \nabla \mu_i$ represents the internal forces due to the presence of non-trivial compositional order parameters, and as such it can also be expressed as a divergence of a stress tensor [22]. In what follows, we report results from hybrid lattice Boltzmann (LB) simulations [23, 33] where Eq. 3 is solved by an LB algorithm, and Eqs. 2 are solved via a finite difference we discuss are generic, the simulations we report in what follows are given in simulation units. While the trends we discuss are generic, the simulations we report in what follows are given in simulation units. While the trends we discuss are generic, the simulations we report in what follows are given in simulation units. While the trends we discuss are generic, the simulations we report in what follows are given in simulation units.


to the wall, with a contact angle of $90^\circ$. We note that droplets need to approach the wall close enough in order to stick: this only happens for above $\Phi > 35\%$.

We start by analysing the flow profile. To do so, we plot the average velocity along $x$ (the velocity direction) as a function of $y$ (the velocity gradient direction). While for low $\Phi$ the profile is approximately parabolic (SI, Fig. S1), the flow becomes plug-like at higher $\Phi$ (see Fig. 1). We note that the velocity of the droplets remains close to that of the fluid throughout the channel.

Pressure-driven flow in these suspensions is therefore strongly non-Newtonian, at least for foam-like structures with large $\Phi$. We can nevertheless define, as in experiments, an apparent viscosity, $\eta_a$, by analysing the throughput flow $Q = \int dy v_x(y)$. A useful quantity is the ratio between $Q$ and the throughput flow of a Newtonian fluid with viscosity $\eta_0$, that of the underlying solvent (when no droplets are present). The inverse of this ratio gives a measure of $\eta_a/\eta_0$. A plot of $\eta_a/\eta_0$ as a function of $\Phi$ for a given value of $\Delta p$ (Fig. 2, inset) shows that viscosity increases sharply and non-linearly with $\Phi$, which is suggestive of jamming as the droplet concentration increases [24, 25]. Our current data, though, do not allow us to conclude whether, for small $\Delta p$, there is a linear regime with a finite albeit large viscosity at any $\Phi$, or whether $\eta_a \rightarrow \infty$ for $\Delta p \rightarrow 0$ above a critical $\Phi_c$, as in jammed granular flow [24, 25].

In Figure 2 we focus instead on the variation of $\eta_a/\eta_0$ with pressure difference, at fixed $\Phi$. For all concentrations, we find strong shear thinning. This behaviour resembles that seen in experiments probing the rheology of emulsions and foams. Remarkably, though, for $\Phi > 50\%$ we find this shear thinning behaviour to be “discontinuous”: in other words, there is a jump in the viscosity for a critical value of the forcing (arrows in Fig. 2), signalling a possible flow-induced nonequilibrium transition. This behaviour contrasts with the smooth (or continuous) shear thinning found in hard colloidal dispersions at intermediate shear rates [1], or in previous simulations of droplet emulsions under shear [11, 13, 14]. Discontinuous shear thinning is observed for $\Delta p = 52.4\%, 54.5\%, 65.4\%$ and 76.3%, with the jump occurring for larger pressure differences as $\Phi$ increases (the trend is approximately linear, see SI, Fig. S3). A viscosity jump is also present for larger system size than in Figure 2 (Fig. S4), while it is absent for non-wetting boundary conditions (Fig. S5).

For sufficiently large $\Phi$, therefore, we can define two viscosity branches, lying either side of the discontinuity. To identify the difference between the left and right viscosity branches, we first characterise how the flow affects droplet shape (Figs. 3a, b). To do so, we compute the semi-axes of the ellipse defined by the inertial tensor of each droplet [20] (see SI). The results point to a clear difference: on the left (high viscosity) branch, the droplet shape is constant over time (Fig. 3a, and SI S5). Suppl.
FIG. 1: Geometry and set-up. (a,b) Snapshots of a droplet suspension of area fraction $\Phi = 54.5\%$ (a), and $\Phi = 76.3\%$ (b). The color code refers to the value of $\sum_i \phi_i$: this is $\sim 2$ for droplets, and $\sim 0$ for the background solvent – values are slightly $< 2$ within boundary droplets due to spreading. (c) Velocity profile of the fluid (solid line) compared to the droplet velocity (filled circles), corresponding to a simulation with $\Phi = 76.3\%$.

FIG. 2: Plot of the relative viscosity of the droplet suspension as a function of $\Delta P$, for five different values of $\Phi$. For large enough $\Phi$ this shear thinning is discontinuous, and arrows denote the discontinuities. The small kinks in the bottom two curves at low $\Delta P$ are not significant, and due to inaccuracies in sampling $\eta$ by time averaging which are larger in that regime. Inset: plot of the apparent viscosity versus $\Phi$ for three different values of $\Delta P$; fits are a guide to the eye.

FIG. 3: (a) Plot of the two semiaxis of the ellipse defined by the inertial tensor of two selected droplets taken from a suspension with $\Phi = 76.3\%$ and $\Delta P = 10^{-5}$. Droplet A belongs to the central array of droplets and is far from the boundary. Droplet B belongs to the array just above the wetting layers of droplets. (b) Same as (a), but for a pressure difference of $\Delta P = 7 \times 10^{-5}$, close to the point at which the viscosity drops sharply. (c) Fluid velocity field and droplet pattern for a suspension with $\Phi = 76.3\%$ and $\Delta P = 3 \times 10^{-6}$. (d) Same as (c), but with $\Phi = 76.3\%$ and $\Delta P = 9 \times 10^{-5}$.

Movie 1); on the right (low viscosity) branch, there are more significant deformations, and, importantly, these display marked variations over time (Fig. 3b, and SI, Fig. S2 and Suppl. Movie 2). We therefore name the left branch ‘hard’, and the right branch ‘soft’. We conclude that the discontinuity in the apparent viscosity shown in Fig. 2 can be interpreted as a transition (or sharp crossover) between a hard phase, where the droplets are effectively rigid, and a soft one, where they are highly deformable.

The hard and soft branches also differ in the flow patterns observed in the steady state. When the average flow along $x$ is subtracted out, the residual flow is mainly limited to gaps between droplets in the hard branch (Fig. 3c), whereas it penetrates more deeply within the droplet interior in the soft branch (Fig. 3d). The larger internal flow in the soft phase arises mainly due to interaction between neighbouring lanes of droplets, and is therefore maximal close to the boundary, where the wetting layer of droplets leads to the largest effective friction with the rest of the suspension.

Closer inspection of the simulation results reveal a further intriguing phenomenon. Consider for example a suspension with $\Phi = 54.5\%$, for $\Delta P = 10^{-5}$ – i.e., just after the drop in viscosity in Fig. 2 (the corresponding dynamics is shown in SI, Suppl. Movie 3). As the flow sets in, the droplets that are initially close to the bound-
ary (droplets a and e in Fig. 4a) stick to the wall and slow down dramatically, while those close to the centre (droplets b, c, and d) undergo a ‘stick-slip’ motion whereby they periodically accelerate and decelerate. The oscillations are visually clear when tracking droplet velocity over time (Fig. 4a); Fourier transforming these data shows they are also very regular (Fig. 4b).

**FIG. 4:** (a) Plots of the droplet velocities as a function of time. Droplets b, c and d belong to the array at the centre of the channel, while droplets a and e belong to the wetting layer. Oscillations in the $x$-component of the droplet velocities are apparent for all droplets except those in the wetting layer, where motion is slow. (b) Fourier transform of the droplet velocities time series: clear peaks are visible, corresponding to the oscillation frequency and its multiples.

Oscillations also occur for other values of $\Phi$ and $\Delta p$, and for larger system size (see SI, Fig. S4 and Table S1): notably, the region in phase space where they do is, in all cases, close to the discontinuity in the viscosity curve. This is reasonable, as we expect that near the discontinuous shear thinning transition there should be hysteresis – similarly to what happens next to a thermodynamic first-order transition. Consequently the suspension can hop between the hard and soft viscosity branches, giving rise to oscillations. An analysis of Suppl. Movie 3 additionally suggests that oscillations correlate well with deformations arising from contact interactions between the wetting layer and the nearest lane of droplets. Thus, each droplet in that array slows down when it first touches one of the droplets in the wetting layer, while it squeezes faster through the gap once it is deformed. This latter microscopic mechanism is consistent with the former explanation that oscillations require proximity to the hard-to-soft transition, because shape deformations – which play a key role in the microscopic argument – define the soft phase. Consistently with these arguments, we observe no transition, and no oscillations, with non-wetting boundary conditions (see SI, Suppl. Movie 4, for a typical example of flow at high $\Phi$ without droplet deformation). The droplet velocity oscillations we observe are qualitatively similar to those found in driven colloidal suspensions close to the glass transition [20], as those, too, correlate well with the gap between flowing and boundary colloids. It would be of interest to ask whether even for the colloidal case oscillations arise close to the discontinuous (shear thickening) transition.

The suspension we have considered up to this point has been monodisperse – all droplets had the same size. Polydispersity is known to strongly affect the behaviour of colloidal systems, for instance in so far as the glass transition is concerned [9]. To explore the effect of polydispersity on discontinuous shear thinning in a selected case, we show in Figure 5a the viscosity curves of a bidisperse suspension (where the droplet radius of one component is twice as large as that of the other). While the suspension still clearly shear thins, with a comparable overall drop in viscosity with respect to the monodisperse case, here no discontinuity can be found, apart from the case of $\Phi = 54.5\%$. For this concentration, we find again oscillations (Fig. 5b), however these are much more irregular than in the monodisperse case. These findings suggest that a sufficiently strong polydispersity smooths out the nonequilibrium transition between the hard and soft phases, turning it into a crossover. The reason is that larger droplets start to deform at a weaker forcing than smaller ones, hence the transition occurs more gradually with respect to the monodisperse case.

**FIG. 5:** Rheology of bidisperse suspensions. (a) Apparent viscosity as a function of $\Delta p$ for three different fixed values of $\Phi$, showing clear shear thinning behaviour. (b) Plot of droplets velocities versus time. Droplets b,c,d and e belong to the droplet array in the centre of the channel, while droplet a belongs to the bottom wetting layer.

In summary, we have shown that the rheology of a suspension of deformable non-coalescing droplets, under a pressure-driven flow entails discontinuous shear thinning behaviour. This discontinuity may be viewed as a nonequilibrium transition between a hard droplet regime, which flows slowly, and a soft droplet phase, which flows much more readily. In the former phase, droplet shape is constant over time; in the latter, it varies significantly as they flow. To observe discontinuous shear thickening, we need large enough concentration, $\Phi$. At a given value of $\Phi$, our physical interpretation of the soft-to-hard transition suggests that a key dimensionless parameter is the capillary number [11–14] denoting the ratio between external forcing and interfacial tension. Close to the transi-
tion, we find sustained oscillations which are reminiscent of those reported previously for hard colloidal systems close to the glass transition [20]. It is tempting to speculate that in both cases oscillations arise due to proximity to a discontinuous transition.

In the future, it would be interesting to recreate discontinuous shear thinning in the lab, by studying the rheology of suspensions of non-coalescing droplets [37]. Theoretically, our findings prompt new questions. For instance, it would be useful to characterise the dependence of the hard-to-soft transition on surface tension. It would also be informative to study the microrheology [38] of our droplet suspensions and see what signatures discontinuous shear thinning leaves there.

Acknowledgements: We thank ERC (COLLDENSE network) and EPSRC (EP/N019180/2) for support.

[30] See Supplemental Material for more details on simulations, and for additional results, Supplementary Figures and Movies, The Supplementary Material also includes Refs. [31][36].
[33] A. Tiribocchi, N. Stella, G. Gonella, and A. Lamura.


