

Modelling the Solubility of H_2S and CO_2 in Ionic Liquids Using PC-SAFT Equation of State

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Natural Gas*





* Reference: Canadian Centre for Energy Information



Gas Processing

Sour Gas

- Sour gas = $H_2S > 5.7 \text{ mg/m}^3$ of NG or (4 ppmv).
- Acid gas removal = 'gas sweetening'.
- Acid gases need to be removed for the following reasons:
 - Corrosion problems.
 - H_2S is toxic and flammable.
 - CO_2 may freeze and cause blockage of pipes.
 - CO_2 has poor heating value.
 - Environmental concerns over CO_2 and H_2S emissions.



40% of the **world's** natural gas reserves are sour.

60% of the Middle Eastern natural gas reserves are sour.

34% of **Russia**'s reserves are sour *.









* Reference: Statistics from the International Energy Agency

Acid Gas Removal Technologies

- Chemical absorption (Amine solvents: e.g. MEA, DEA, MDEA)
- Physical absorption (e.g. Selexol, purisol and ionic Liquids)
- Adsorption (e.g. Molecular sieve zeolite and activated charcoal)
- Membranes (polymer based e.g. cellulose acetate, polyamides)
- Cryogenic Distillation (CFZ, Sprex)
- Hybrid Technologies



Cryogenic separation



Membranes





Amine processes



Molecular sieve zeolite

Aims



Improve the pre-existing amine units for sour gas treatment

Explore the use of Ionic liquids as an alternative solvent

Thermodynamic model

Represent the solubility of CO₂ and H₂S in ILs

Effect of accounting for ILs association and charge on the solubility

Find the best strategy and association scheme



Ionic Liquids (ILs): Common cations and anions



ILs are materials consisting of ions and are liquid below 100°C. They are salts in the liquid state.



* Reference: Somers, A.E.; Howlett, P.C.; MacFarlane, D.R.; Forsyth, M. Lubricants 2013, 1, 3-21.



Ionic Liquids (ILs): Features

• Easy to separate

• Very low vapour pressure (negligible volatility)

• Non-flammable

- High thermal stability
- Low toxicity
- Structural tunability
- Recyclable and reusable



Thermodynamic Modelling: Previous models





Thermodynamic Modelling:

Perturbed-Chain Statistical Associating Fluid Theory PC-SAFT





$$a^{residual} = a^{hardchain} + a^{dispersion} + a^{association} + a^{electrolyte}$$

* Reference : J. Gross, G. Sadowski, Ind. Eng. Chem. Res. 40 (4) (2001) 1244–1260.

Association: Hydrogen Bonding



1-hexyl-3-methylimidazolium bis(trifluoromethanesulfonyl)amide, $[C_6 mim]^+[NTf_2]^-$



Strategies and Association schemes for ILs

Strategies: Two strategies were investigated



Association schemes: The investigated association schemes

2-site association scheme 2(1:1) = One donor and one acceptor

3-site association scheme 3(2:1) = Two donor and one acceptor

4-site association scheme 4(2:2) = Two donor and two acceptor



ILs pure component parameters Experimental density fit





Solubility of acid gases in C_nmimNTf₂ ILs as a molecule and electrolyte (best association scheme)



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Conclusions



- ILs could contribute significantly to improving the economy and environmental sustainability of the AGR process.
- The solubility of acid gases in ILs can be accurately described using PC-SAFT by accounting for the self-association between IL molecules and selecting the proper association scheme.
- No binary interaction parameters are needed.
- Although no significant improvement has been achieved by treating ILs as electrolytes, the model predictive capability is enhanced.
- H_2S is about two times more soluble than CO_2 in the studied ILs.
- The solubility of acid gases in ILs increases by increasing the cation alkyl chain length of the ILs. Therefore, of the studied ILs; [C₈mim][NTf₂] is the most promising solvent for AGR applications especially for high H₂S content NG.

Future Work



- Explore the applicability of PC-SAFT model for multicomponent natural gas systems (methane, acid gases, water, ethanolamines and ILs).
- Build IL-based gas treatment process simulation using our PC-SAFT parameters for the studied ILs.
- Evaluation of the proposed gas treatment process against current conventional techniques.

Acknowledgement





Libyan Ministry of Higher Education and Scientific Research

